

Control Design Based on Limited Plant Model Information with Applications to Power Systems

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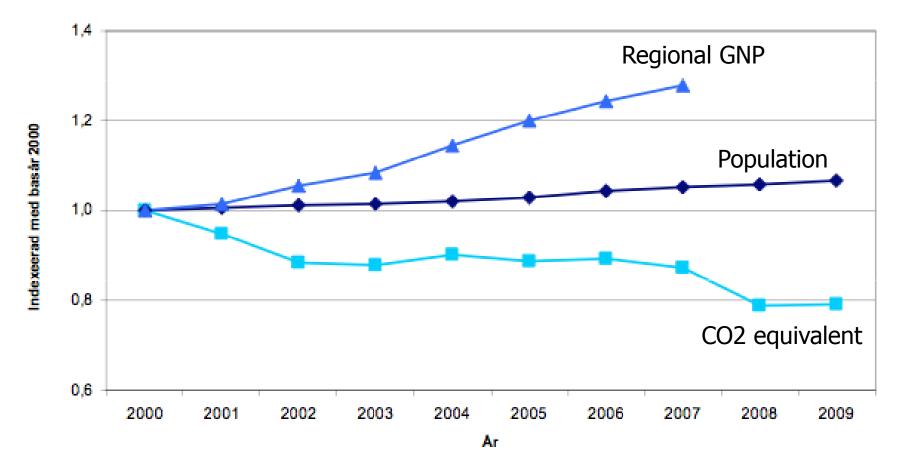
Joint work with Farhad Farokhi and Cédric Langbort



Workshop on Dynamics, Control and Pricing in Power Systems, Lund, May 18-20, 2011



Stockholm Challenge



Stockholm Royal Seaport

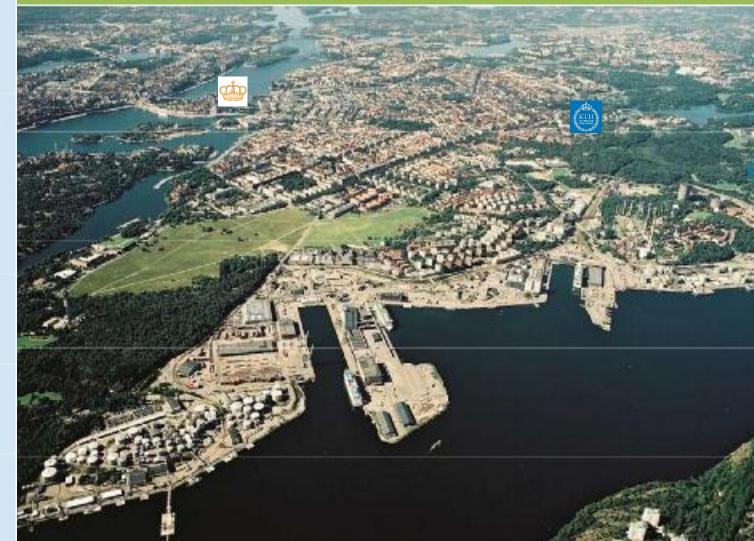
2010

- Oil depot
- Container terminal
- Ports
- Gas plant

2030

- I0,000 new homes
- 30,000 new work spaces
- 600,000 m2 commercial space
- Modern port and cruise terminal
- 236 hectares sustainable urban district
- Walking distance to city centre

From a brown field area to a sustainable city district



Stockholm Royal Seaport

2010

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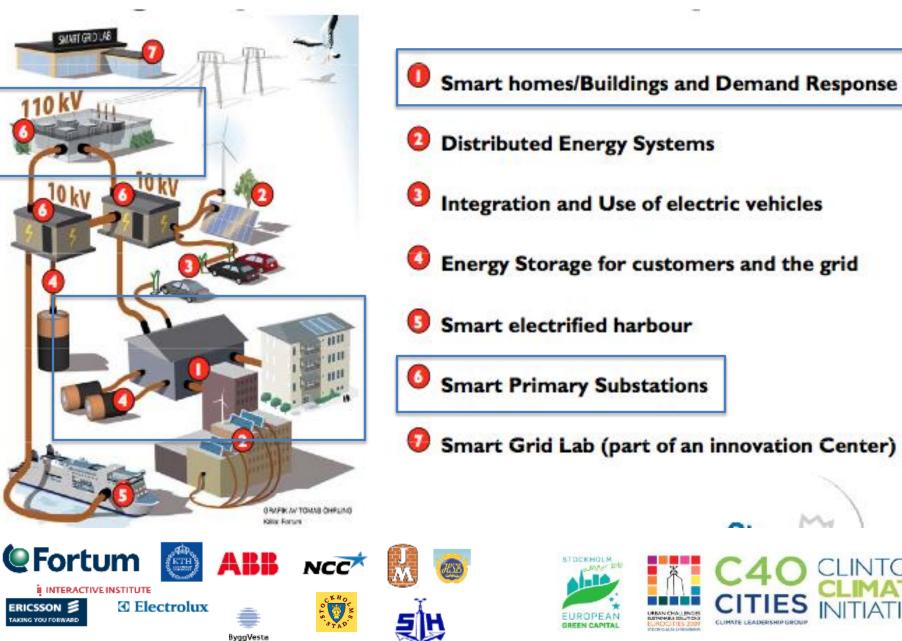
2030

- 10,000 new homes
- 30,000 new work spaces
- 600,000 m2 commercial space
- Modern port and cruise terminal
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From a brown field area to a sustainable city district



Smart Grid in the Stockholm Royal Seaport



Two Royal Seaport Projects

- Smart grid communications over 4G LTE
 - Can power grid control loops be closed over the mobile communication infrastructure?



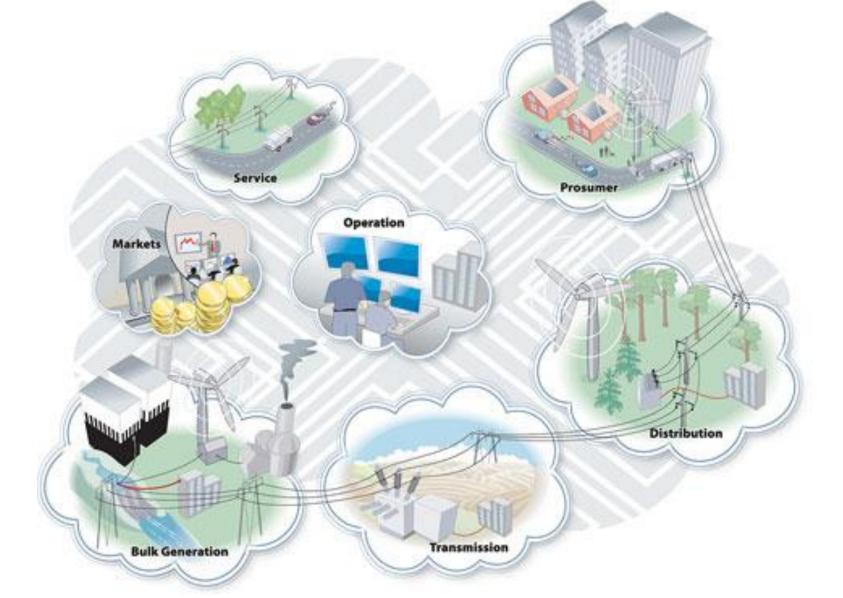


- Appliance scheduling and storage in smart buildings
 - Control architecture and mechanisms for demand-response





From Centralized to Distributed Control



Example

$$x_1(k+1) = a_{11}x_1(k) + a_{12}x_2(k) + u_1(k)$$

$$x_2(k+1) = a_{21}x_1(k) + a_{22}x_2(k) + u_2(k)$$

Keep J small, when

• Controller 1 knows a_{11} and a_{12}

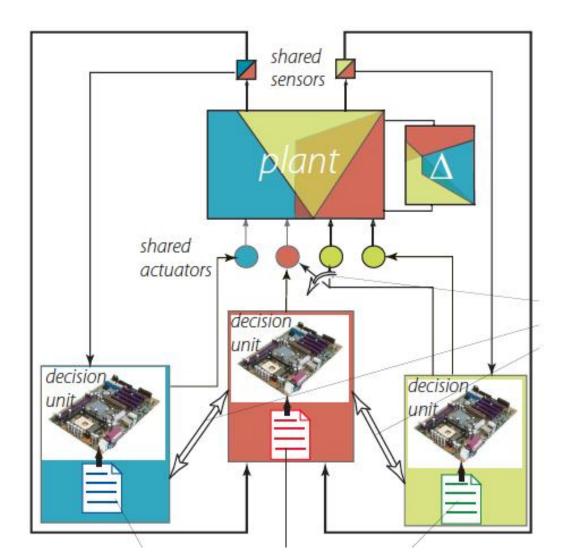
$$J = \sum_{k=1}^{\infty} \|x(k)\|^2 + \|u(k)\|^2$$

• Controller 2 knows a_{21} and a_{22}

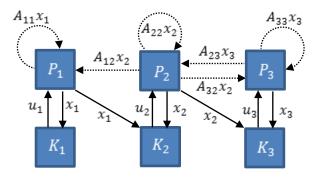
$$u_1(k) = -a_{11}x_1(k) - a_{12}x_2(k)$$
 achieves $J \le 2J^*$
$$u_2(k) = -a_{21}x_1(k) - a_{22}x_2(k)$$

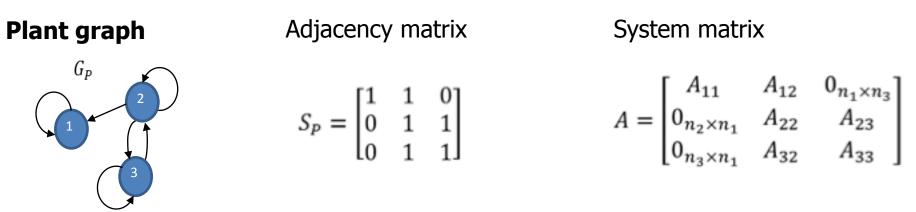
No limited plant model information strategy can do better.

Distributed Control with Limited Model Information



Plant

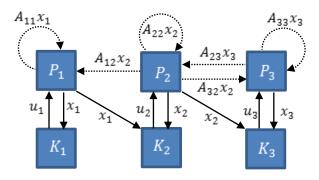


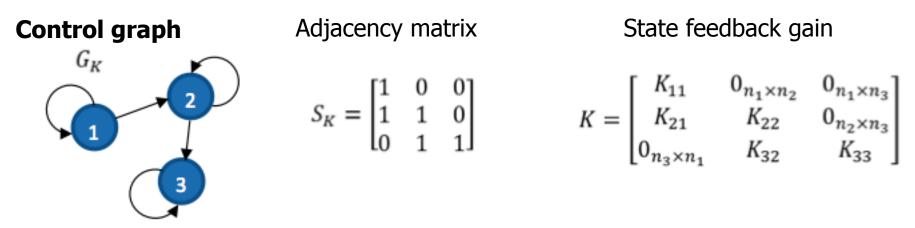


Plant

$$\begin{split} P &= (A, B, x_0) \in \mathcal{A} \times \mathcal{C} \times \mathcal{X} \\ \mathcal{A} &= \{ A \in R^{n \times n} | A_{ij} = 0 \in R^{n_i \times n_j} \text{ for all } 1 \leq i, j \leq q \text{ such that } (s_P)_{ij} = 0 \} \\ \mathcal{C} &= \{ B \in R^{n \times n} \mid \underline{\sigma}(B) \geq \epsilon, B_{ij} = 0 \in R^{n_i \times n_j} \text{ for all } 1 \leq i \neq j \leq q \} \\ x_i(k+1) &= A_{ii} x_i(k) + \sum_{j \neq i} A_{ij} x_j(k) + B_{ii} u_i(k) \\ x_i \in R^{n_i} \text{ and } u_i \in R^{n_i} \end{split}$$

Controller



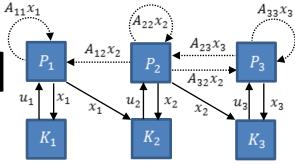


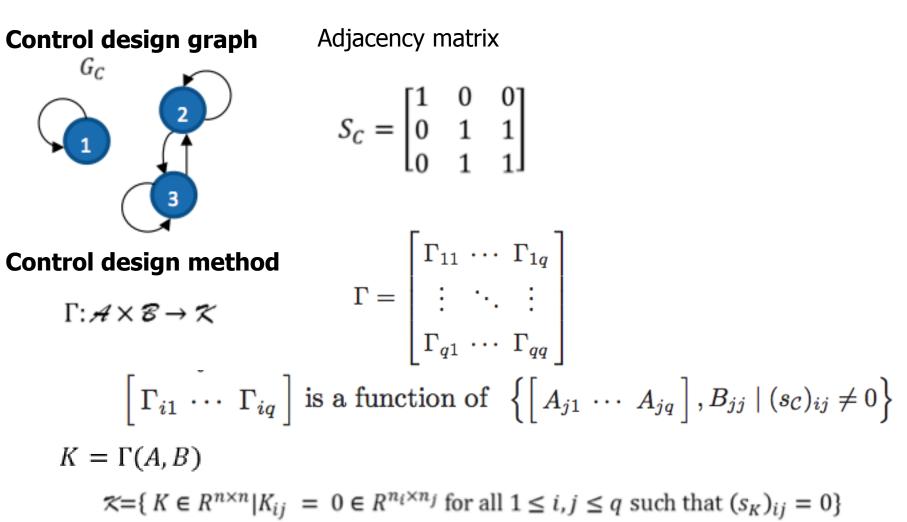
Controller

$$u(k) = Kx(k)$$

$$\approx = \{ K \in \mathbb{R}^{n \times n} | K_{ij} = 0 \in \mathbb{R}^{n_i \times n_j} \text{ for all } 1 \le i, j \le q \text{ such that } (s_K)_{ij} = 0 \}$$

Control Design Method

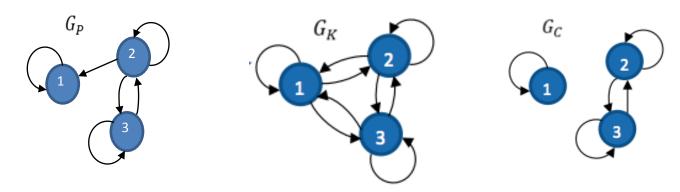




Performance metric

$$J_P(K) = \sum_{k=1}^{\infty} x(k)^T Q x(k) + \sum_{k=0}^{\infty} u(k)^T R u(k)$$

given



Assumptions

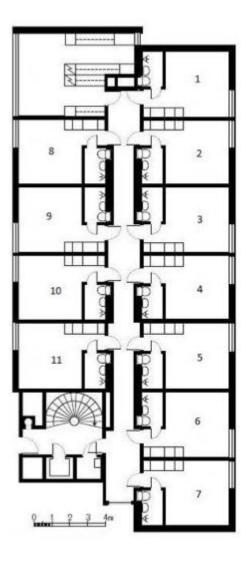
• $\mathscr{B} = \{B \in \mathbb{R}^{n \times n} \mid \underline{\sigma}(B) \ge \epsilon, B_{ij} = 0 \in \mathbb{R}^{n_i \times n_j} \text{ for all } 1 \le i \ne j \le q\}$

is a set of diagonal matrices

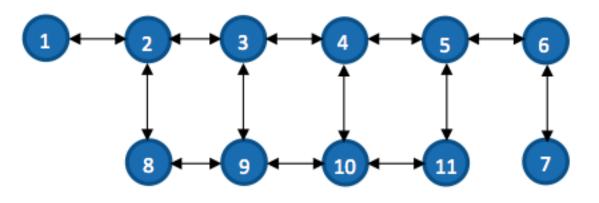
- G_K is a complete graph
- Q = R = I.
- for every plant $P = (A, B, x_0) \in \mathcal{P}$, there

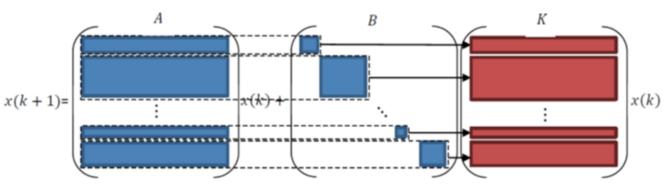
exists an optimal controller $K^*(A, B) \in \mathcal{K}$ such that $J_P(K^*(A, B)) \leq J_P(K)$, for all $K \in \mathcal{K}$

Motivating HVAC Example



Plant graph





Competitive Ratio and Dominance

The **competitive ratio** of a control design method $\Gamma: \mathcal{A} \times \mathcal{B} \to \mathcal{K}$

$$r_{\mathcal{P}}(\Gamma) = \sup_{P=(A,B,x_0)\in\mathcal{P}} \frac{J_P(\Gamma(A,B))}{J_P(K^*(P))}$$

 Γ dominates another control design method Γ' if

 $J_P(\Gamma(A,B)) \le J_P(\Gamma'(A,B)), \quad \forall P = (A,B,x_0) \in \mathcal{P},$

Deadbeat Control

The deadbeat control design method $\Gamma^{\Delta} : \mathcal{A}(S_{\mathcal{P}}) \times \mathcal{B}(\epsilon) \to \mathcal{K}$ is $\Gamma^{\Delta}(A, B) = -B^{-1}A, \text{ for all } P = (A, B, x_0) \in \mathcal{P}$

The control design for subsystem i depends only on subsystem i's controller gains:

$$\left[\Gamma_{i1}(A,B) \Gamma_{i2}(A,B) \cdots \Gamma_{iq}(A,B)\right] = B_{ii}^{-1} \left[A_{i1} A_{i2} \cdots A_{iq}\right]_{G_{\mathcal{C}}}$$

Lemma Suppose $G_{\mathcal{P}}$ contains no isolated node. Then,

$$r_{\mathcal{P}}(\Gamma^{\Delta}) = 1 + 1/\epsilon^2$$

The performance of the deadbeat control design method is at most $1 + 1/\epsilon^2$, times the performance of the optimal control design method as

$$r_{\mathcal{P}}(\Gamma) = \sup_{P=(A,B,x_0)\in\mathcal{P}} \frac{J_P(\Gamma(A,B))}{J_P(K^*(P))}$$

Cheap Control

For the performance metric

$$J_P(K) = \sum_{k=1}^\infty x(k)^T Q x(k) + \sum_{k=0}^\infty u(k)^T R u(k)$$

the competitive ratio

$$r_{\mathcal{P}}(\Gamma) = \sup_{P=(A,B,x_0)\in\mathcal{P}} \frac{J_P(\Gamma(A,B))}{J_P(K^*(P))}$$

is

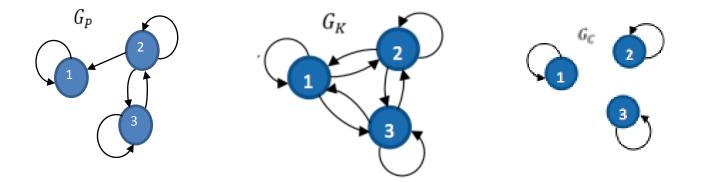
$$r_P(\Gamma^{\Delta}) = 1 + \overline{\sigma}(R) / (\underline{\sigma}(Q)\epsilon^2)$$

Hence, as $\overline{\sigma}(R)/\underline{\sigma}(Q)$ goes to zero, the LQ controller converges to deadbeat.

Competitive Ratio

Theorem Suppose $G_{\mathcal{P}}$ has no isolated node, G_K is a complete graph, and and $G_{\mathcal{C}}$ is totally disconnected. Then, the competitive ratio of any control design method $\Gamma \in \mathcal{C}$ satisfies

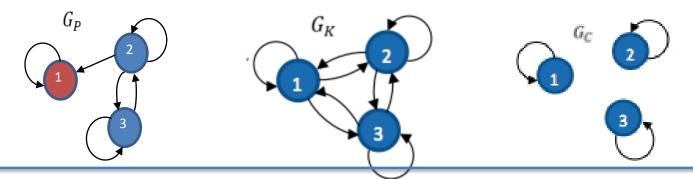
 $r_{\mathcal{P}}(\Gamma) \ge 1 + 1/\epsilon^2$



$$r_{\mathcal{P}}(\Gamma) = \sup_{P=(A,B,x_0)\in\mathcal{P}} \frac{J_P(\Gamma(A,B))}{J_P(K^*(P))}$$

Deadbeat is Undominated

Theorem Suppose $G_{\mathcal{P}}$ has no isolated node, $G_{\mathcal{K}}$ is a complete graph, and and $G_{\mathcal{C}}$ is totally disconnected. Then, deadbeat is undominated if and only if $G_{\mathcal{P}}$ has no sink

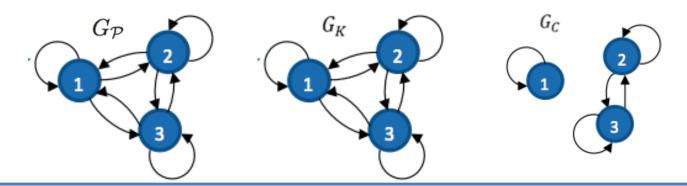


If $G_{\mathcal{P}}$ has one or more sinks, then the control method should be modified to do "local optimal control" for each sink and deadbeat for the other nodes.

Influence of Design Information

Theorem Suppose $G_{\mathcal{P}}$ and $G_{\mathcal{K}}$ are complete graphs. If $G_{\mathcal{C}} \neq G_{\mathcal{P}}$ then

 $r_{\mathcal{P}}(\Gamma) \ge 1 + 1/\epsilon^2$



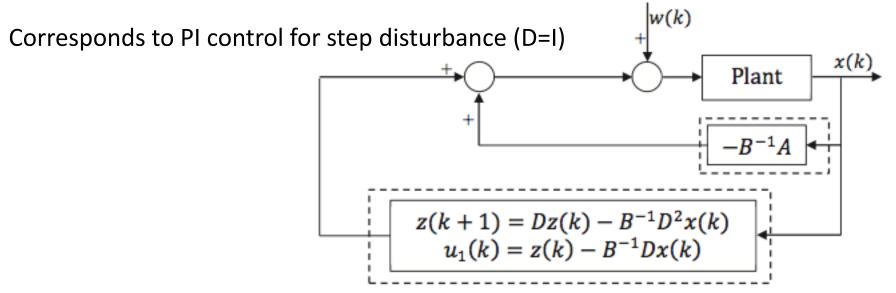
Achieving a better competitive ratio than the deadbeat design strategy requires each subsystem to have full knowledge of the plant model in the design of each subcontroller.

Servomechanism Design

Extensions to plant with disturbance:

$$egin{aligned} x(k+1) &= Ax(k) + B(u(k)+w(k)) \; ; \; x(0) = x_0, \ w(k+1) &= Dw(k) \; ; \; w(0) = w_0 \end{aligned}$$

Deadbeat controller with deadbeat observer



Conclusions

- Smart energy systems often lead to distributed control problems with limited information exchange
- Considered the role of plant model information
- Achievable performance in terms of competitive ratio can be derived for certain cases
- Provides insights on control information topologies (not necessarily design)



http://www.ee.kth.se/~kallej

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- F. Farokhi, C. Langbort, and K. H. Johansson, "Control design with limited model information," American Control Conference, 2011.

